

Hydromechanics

— hydrostatic
— hydrodynamics

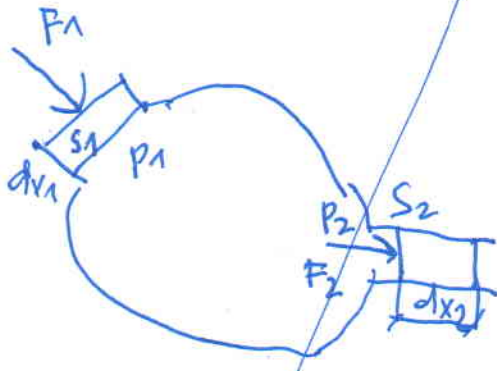
fluid — liquid
 — gas
 — plyu

Pressure $p = \frac{dF}{dS} \quad \left[\frac{N}{m^2} = Pa \right]$

$\vec{F} = \int_S p d\vec{S} \quad [N]$

33. Pascal's principle

External force



$dW_1 = F_1 \cdot dx_1 = p_1 \cdot (S_1 \cdot dx_1) = p_1 dV_1$

$dW_2 = F_2 \cdot dx_2 = p_2 \cdot S_2 dx_2 = p_2 dV_2$

$dW_1 = dW_2$

$p_1 dV_1 = p_2 dV_2$

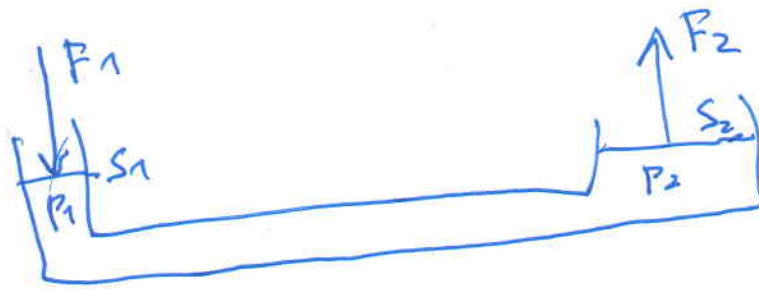
incompressible
[inkomprimibil]
neklasticky

$p_1 = p_2$

The pressure due to an external force is in the whole volume the same.

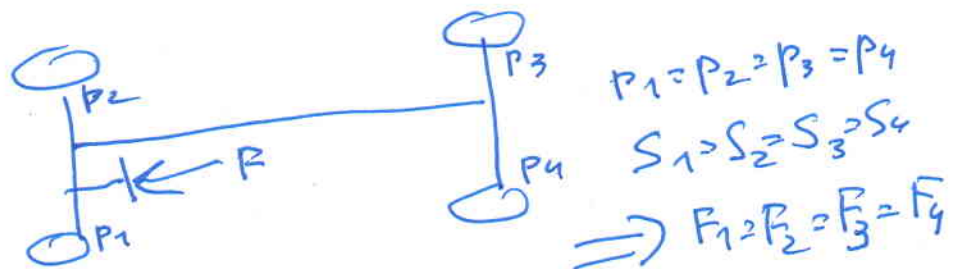
For gas is valid the same

Use - hydraulic press



$$\begin{aligned}
 P_1 &= P_2 \\
 \frac{F_1}{S_1} &= \frac{F_2}{S_2} \quad \Rightarrow \quad F_2 = F_1 \cdot \frac{S_2}{S_1} \quad \text{ratio}
 \end{aligned}$$

hydraulic brake system

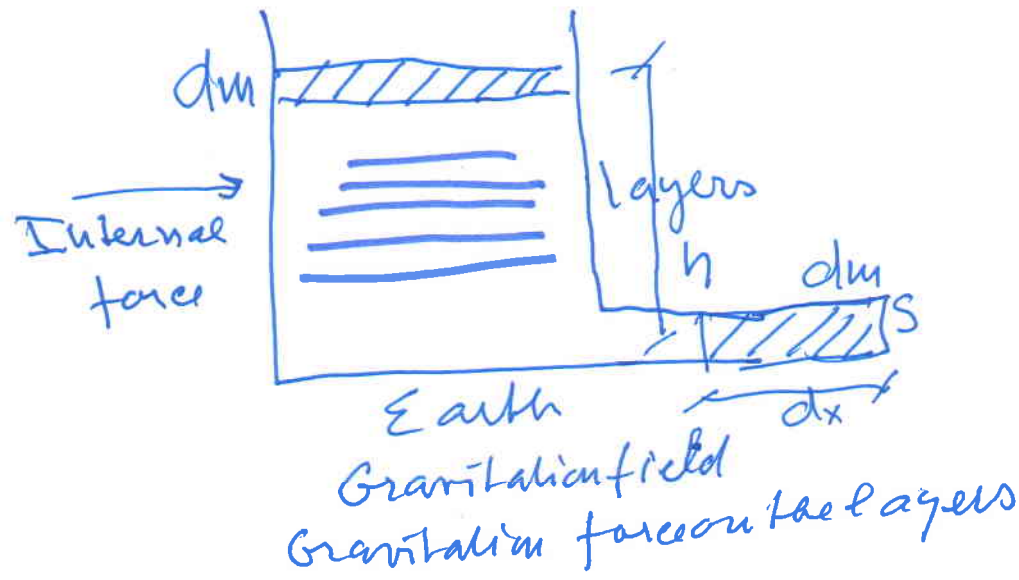


brake pads
brzdové destičky

$\Rightarrow$ The car doesn't skid

34. Hydraulic pressure

Due to an internal forces (in gravitation field)



$$dmgh = dW = F \cdot dx = p \cdot \underbrace{S \cdot dx}_{dV}$$

$$dmgh = p \cdot dV$$

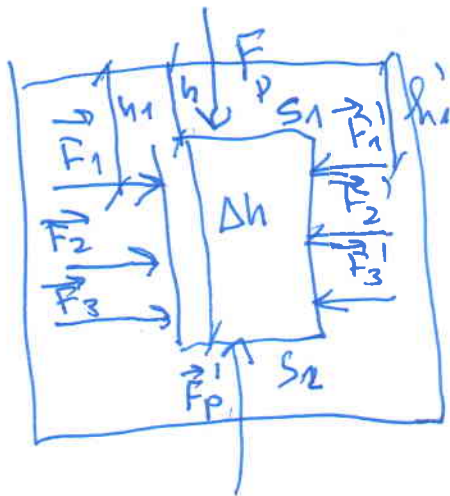
$$P_h = h \rho g$$

Hydraulic pressure

In liquid

In gas

35. Archimede's principle



$$\begin{aligned}
 S_1 &= S_2 = S \\
 \vec{F}_1 &= -\vec{F}_1' \\
 h_1 &= h_1' \\
 \vec{F}_2 &= \vec{F}_2' \\
 \vec{F}_3 &= \vec{F}_3'
 \end{aligned}
 \left. \begin{array}{l} \\ \\ \\ \end{array} \right\} \begin{array}{l} u_1 = u_1' \\ \sum \vec{F} = 0 \end{array}$$

F_{V2} Buoyant force madnâşirâ şik
 [13 buoyant]

$$F_{V2} = F_p - F_p' = pS_1 - p'S_2$$

$$F_{V2} = h_1 p g S - (h_1 + \Delta h) p g S$$

$$F_{V2} = \cancel{h_1 p g S} - \cancel{h_1 p g S} - \Delta h \cdot S \cdot p g$$

$$F_{V2} = - \rho g V$$

Archimede's principle

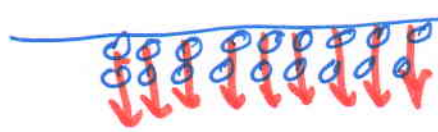
The buoyant force on a body has the same magnitude as the weight of the ~~body~~ body push up and opposite direction as gravitation force.
 is valid for gas too

36. Surface tension

[Energy]

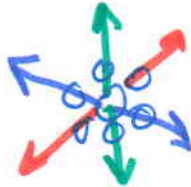
Povrchová napětí

$$\Rightarrow \sigma = \frac{F}{l} \left[\frac{N}{m} \right]$$

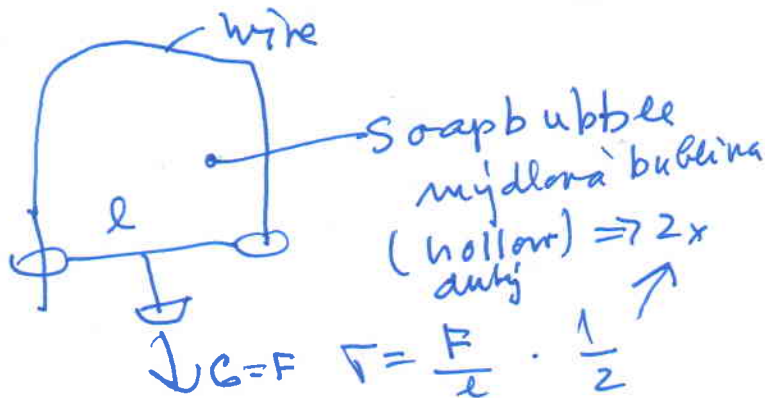


the last line

molecules in the last line are only under forces down

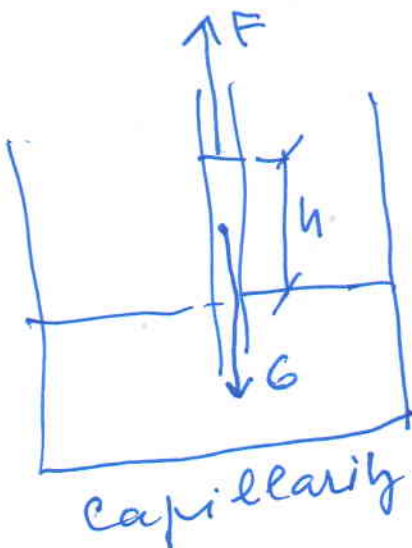


The internal molecules are in equilibrium
 $\sum F = 0$



$$\sigma = \frac{F}{l} \cdot \frac{dr}{dr} = \frac{dW}{dS} = \frac{dE}{dS} \left[\frac{J}{m^2} \right]$$

area's density of Energy
 Povrchová hustota energie



$$G = F$$

$$(\pi R \cdot h) \cdot \rho \cdot g = \sigma \cdot l = \sigma \cdot 2\pi r$$

$$\Rightarrow \angle \sigma$$

37. equation of continuity

We use streamlines to describe
 prondeni'cay

- laminar
 - turbulent
 [turbulent]



Laminar



Turbulent

Continual flow

Unakeni prondeni'

velocity
 pressure
 temperature

At a given
 location,
 doesn't change
 with time

Volume flow

$$Q_v = \frac{dV}{dt} \left[\frac{m^3}{s} \right]$$



$$Q_v = \frac{S \cdot dl}{dt} = S \cdot v$$

$$Q_v = S \cdot v$$

Mass flow

$$Q_m = \frac{dm}{dt} = \frac{\rho \cdot dV}{dt} = \rho \cdot S \cdot v$$

$$Q_m = \rho \cdot S \cdot v \left[kg \cdot s^{-1} \right]$$

1) Incompressible fluid (= liquid)

Law of conservation of mass



Manometry
tubing
meromethane p.

medium
doesn't even rise

medium doesn't
even get lost

$$Q_{V1} = Q_{V2}$$

$$S_1 \cdot v_1 = S_2 v_2$$

Equation of
continuity
for incompressible
fluid

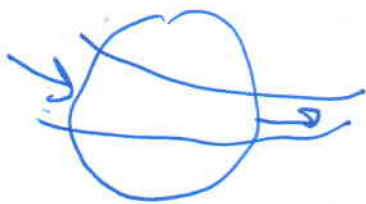
2, compressible fluid (gas)

$$Q_{m1} = Q_{m2}$$

$$\rho_1 S_1 v_1 = \rho_2 S_2 v_2$$

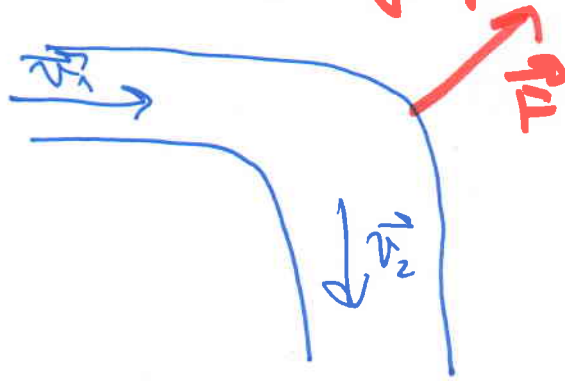
Equation of
continuity
for compressible
fluid

3, generally



$$\oint \rho v dS = 0$$

38. Principle of fluid momentum



Impulse of force

$$\vec{I} = \vec{F} \cdot \Delta t = \Delta \vec{p} = \Delta m (\vec{v}_2 - \vec{v}_1) / \Delta t$$

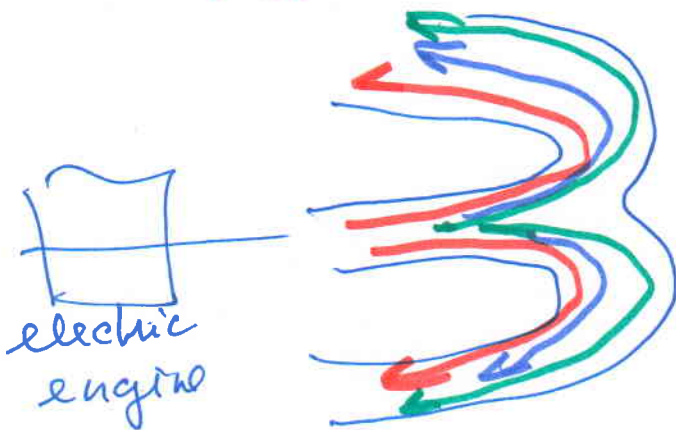
$$\vec{F} = \frac{\Delta m}{\Delta t} (\vec{v}_2 - \vec{v}_1)$$

$$\boxed{\vec{F} = Q_m \cdot (\vec{v}_2 - \vec{v}_1)}$$

Vector difference

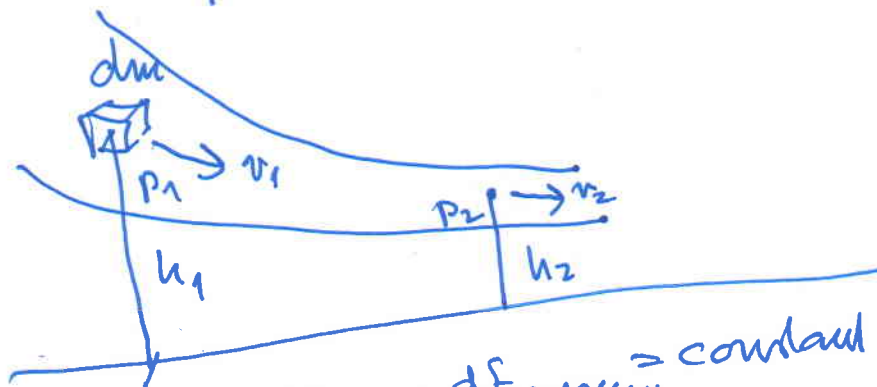
Fluid action by force on a body (tube), depends on mass flow Q_m and change of velocity vectors $(\vec{v}_2 - \vec{v}_1)$

Pelton turbine



39. Bernoulli's equation

Law of conservation of Energy



$$dE_k + dE_p + dE_{\text{pressure}} = \text{constant}$$

kinetic potential pressure

$$\frac{1}{2} dm \cdot v^2 + dmgh + PdV = \text{constant} / dV$$

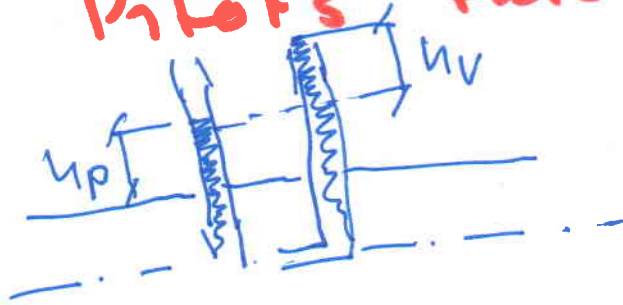
$$\frac{1}{2} \rho v^2 + \rho gh + p = \text{constant}$$

Bernoulli's eq.

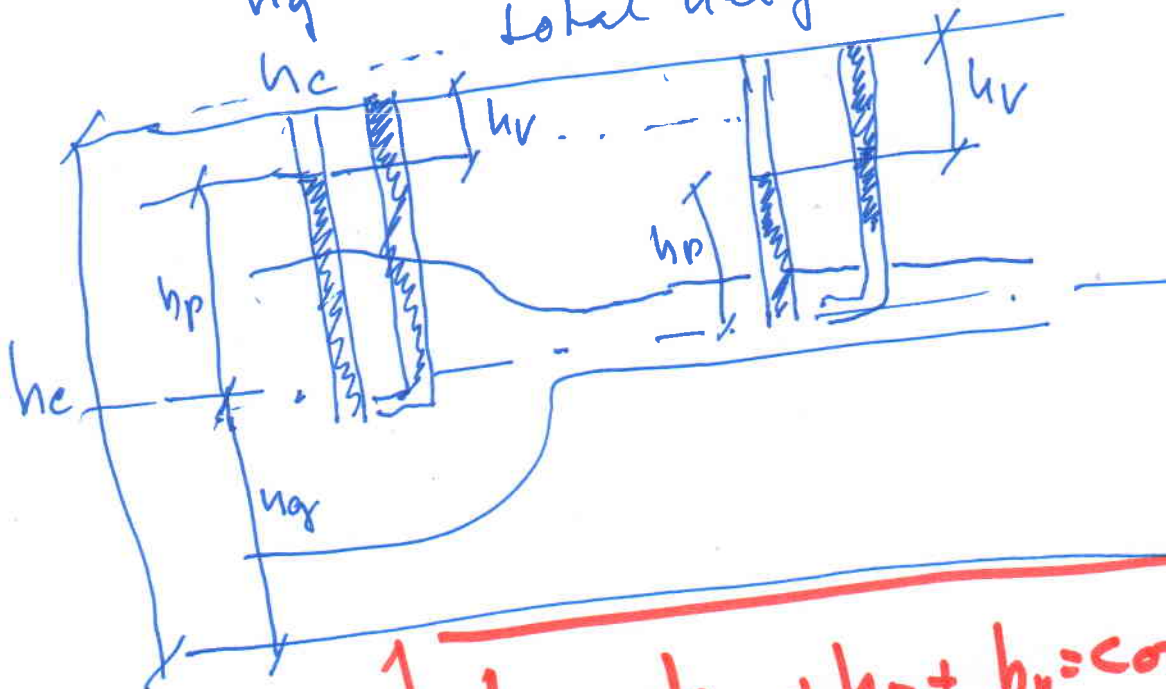
Or

$$\frac{1}{2} \rho v_1^2 + \rho gh_1 + p_1 = \frac{1}{2} \rho v_2^2 + \rho gh_2 + p_2$$

Pilot's tube



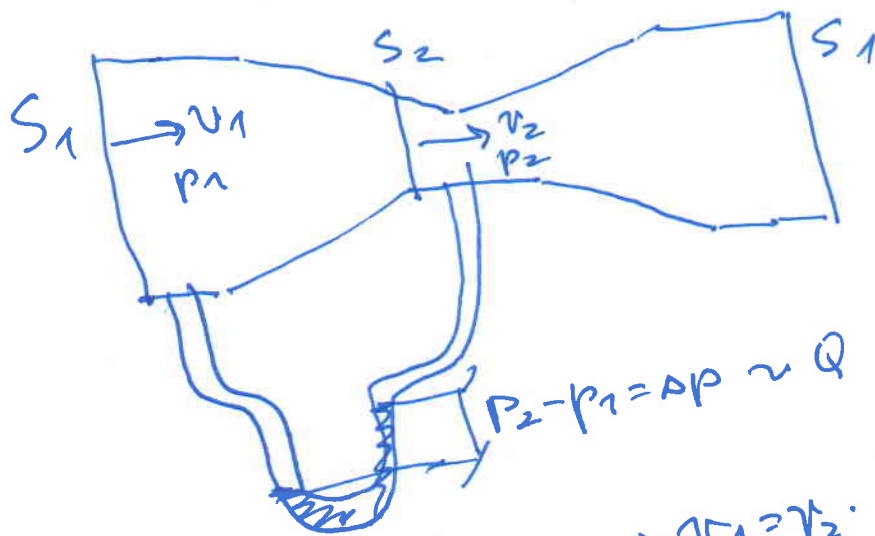
h_v ... velocity height
 h_p ... pressure height
 h_q ... conventional height
 Total height



$$h_c = h_q + h_p + h_v = \text{constant}$$

Bernoulli's equation
Height equation

Venturi's tube



$$S_1 v_1 = S_2 v_2 \quad \rightarrow v_1 = v_2 \cdot \frac{S_2}{S_1}$$

$$\frac{1}{2} \rho v_1^2 + p_1 + \cancel{h_1 \rho g} = \frac{1}{2} \rho v_2^2 + p_2 + \cancel{h_2 \rho g}$$

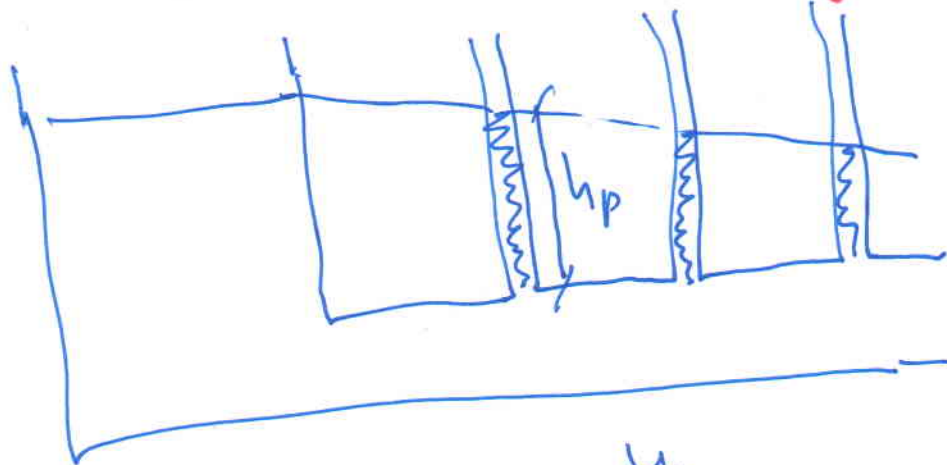
$$\frac{1}{2} \rho v_2^2 \frac{S_2^2}{S_1^2} + p_1 = \frac{1}{2} \rho v_2^2 + p_2 \quad h_1 = h_2$$

$$\frac{1}{2} \rho \left(\frac{S_2^2}{S_1^2} - 1 \right) \cdot v_2^2 = p_2 - p_1$$

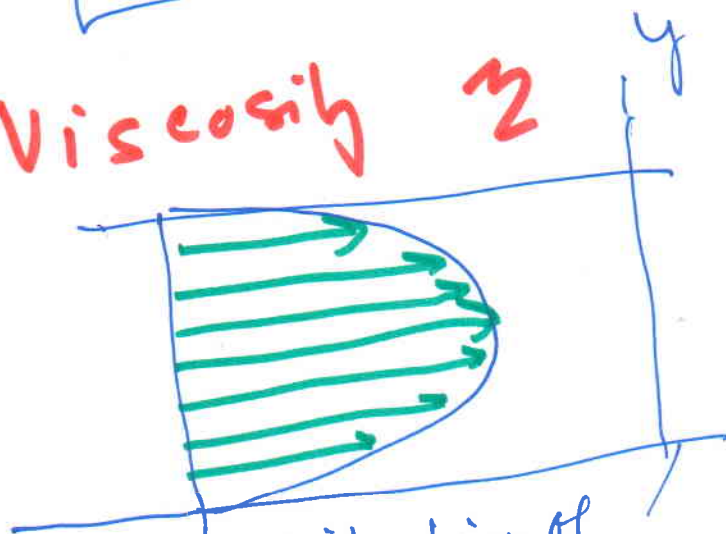
$$v_2 = \sqrt{\frac{(p_2 - p_1) \cdot 2}{\rho \left(1 - \frac{S_2^2}{S_1^2} \right)}}$$

$$Q_v = S_2 \cdot v_2 \quad \rightarrow \text{Quantity of volume flow}$$

Motion of real fluid (liquid)



Viscosity η



distribution of

velocities

due to friction among layers

The velocity at the wall is $\rightarrow$ zero

τ -- tangential stress

$$\tau = \frac{F}{S} \left[\frac{N}{m^2} \right]$$

$$\tau = \eta \cdot \frac{dv}{dy}$$

$$\boxed{\eta = \tau \cdot \frac{1}{\frac{dv}{dy}} \text{ [Pa.s]}}$$

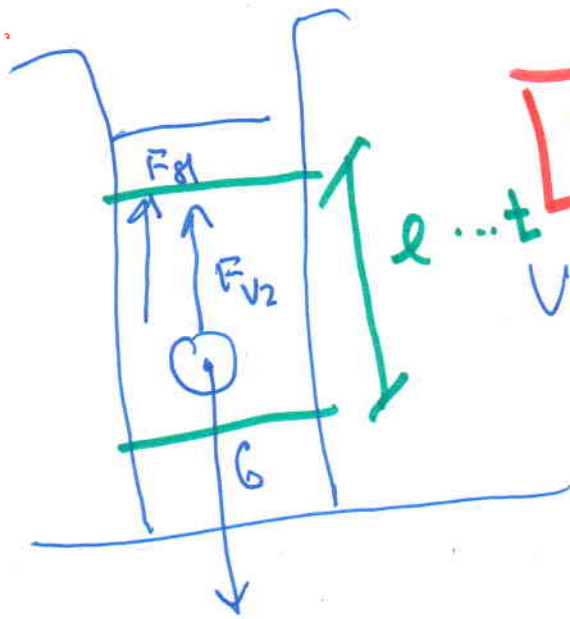
dynamic
viscosity

η is the tangential force per unit area of fluid which resists the motion of one layer over another.

Body shape $\bigcirc \supset \mid \subset$ - hemisphere
 Stokes' formula for sphere
 $V = \frac{4}{3}\pi r^3$

$$F_H = 6\pi \eta \cdot v \cdot r$$

Stoke's viscometer



$$F_{H2} + F_{H1} = G$$

$$V\rho g + 6\pi \eta \cdot v \cdot r = \frac{4}{3}\pi r^3 \rho g$$

$\Rightarrow v = \text{counted}$